

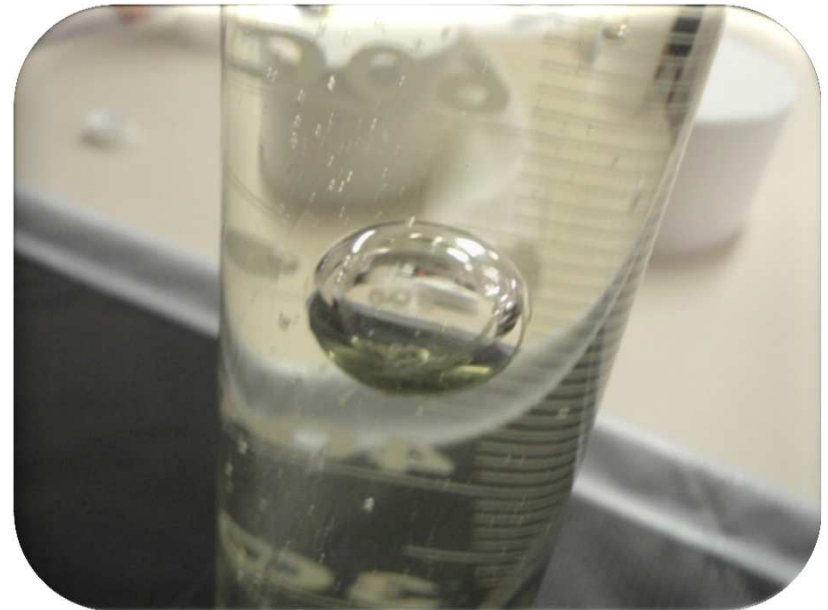
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Problem 16

Rising bubble

reporter:

Ibraim Rebouças





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Problem 16: Rising bubble

Problem 16

Rising bubble

A vertical tube is filled with a **viscous fluid**. On the bottom of the tube, there is a **large air bubble**. Study the bubble rising from the bottom to the surface.

Contents

Theoretical introduction

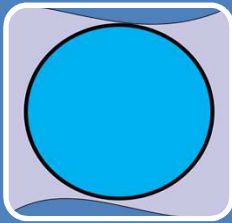
- Kinds of bubble
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- Drag forces
- Lateral Flow
- Rise velocity
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- Influence of the temperature

Experiments

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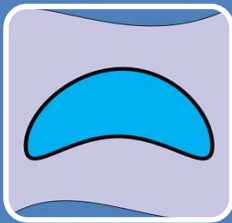
Conclusion

Kinds of bubbles



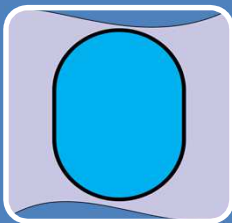
Spherical bubble

- Very viscous fluids.
- Governed by Stokes law



Spherical cap bubble

- Stable to moderate viscous fluids.



Taylor's bubble

- Height bigger than the diameter of the pipe.
- Constant velocity for all volumes.

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The phenomenon



Viscosity

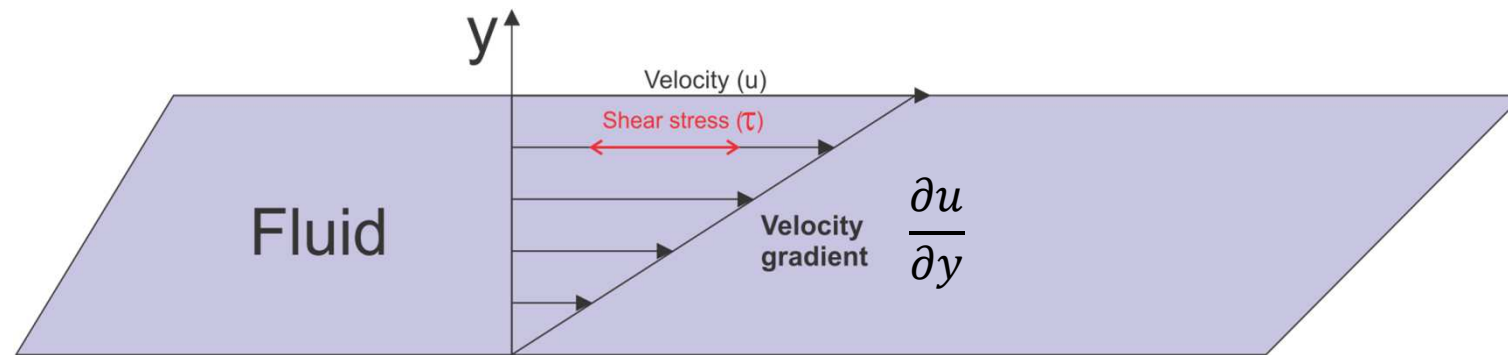
- It's the measurement of the resistance to a shear stress.

The viscosity is measured by a coefficient.

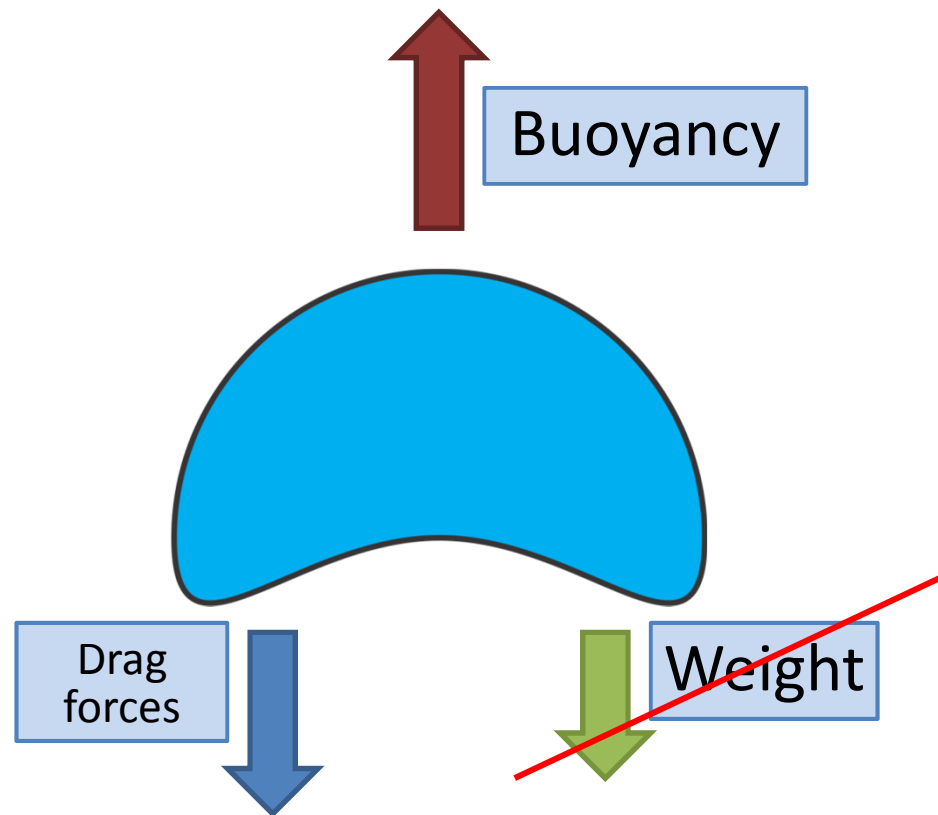
μ is called absolute viscosity coefficient.

Kinematic viscosity $\nu = \frac{\mu}{\rho}$ ρ is de density of the fluid

$$\tau \propto \frac{\partial u}{\partial y} \Rightarrow \tau = \mu \frac{\partial u}{\partial y}$$



Forces acting on the bubble



Forces acting on the bubble

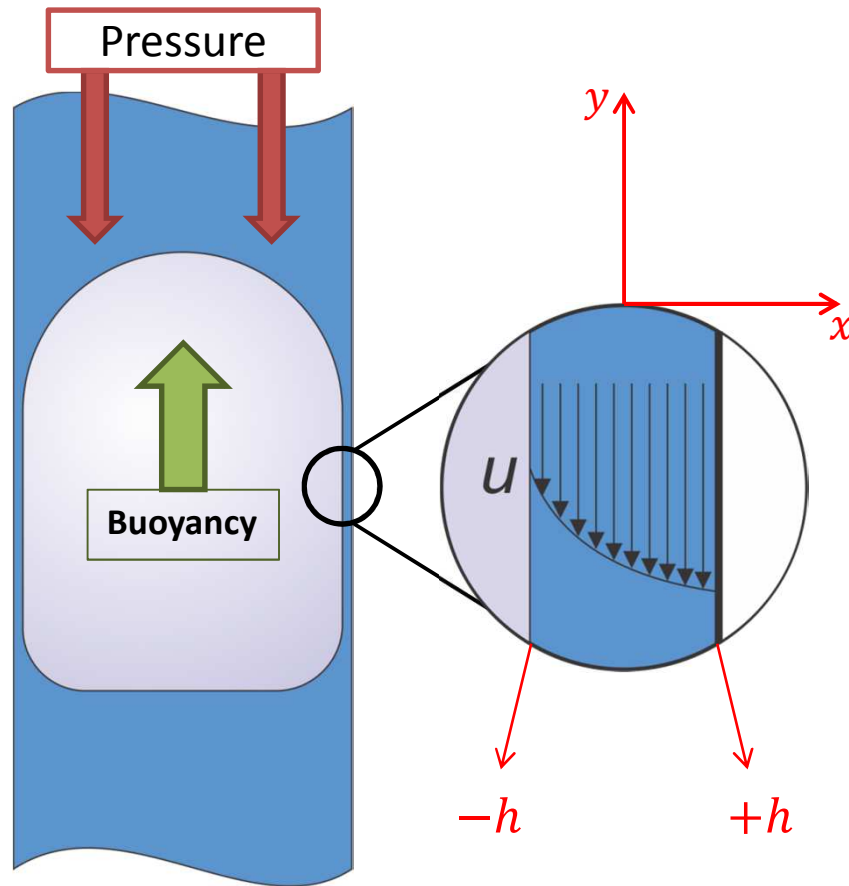
~~$$\text{Newton's equation}$$
$$F_d = \frac{1}{2} A \rho U^2 C_d$$~~

~~$$\text{Stokes' drag}$$
$$F_d = -bv$$~~

A red arrow points from the center of the two crossed-out equations down to the text below.

Both are wrong, because they do not consider the boundary effects.

Border of the bubble

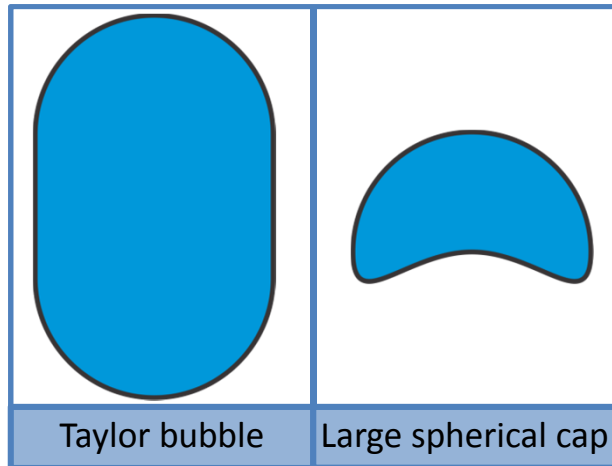


We must have conservation of mass for the liquid ahead and behind the bubble.

$$\mu \frac{d^2 u}{dx^2} = \frac{\partial p}{\partial y} = \text{constant} < 0$$

$$u = -\frac{dp}{dy} \frac{h^2}{2\mu} \left(1 - \left[\frac{x}{h} \right]^2 \right)$$

Large spherical cap or Taylor bubble velocity



- The velocity is constant and does not depend on the volume of the bubble.

For Taylor bubble or large spherical cap bubbles, the velocity can be described by the following equation:

$$\frac{U}{\sqrt{gD}} = -\frac{8}{3} \frac{\nu}{\sqrt{gD^3}} + \frac{\sqrt{2}}{3} \left(1 + \frac{32\nu^2}{gD^3} \right)^{1/2}$$

Annotations: A box labeled 'Terminal velocity (m/s)' points to 'U'. A box labeled 'Diameter of the bubble' points to 'D'.

For low viscosity fluids (e.g. Water), the equation can be written as:

$$U = \frac{\sqrt{2}}{3} \sqrt{gD}$$

Spherical cap bubbles

- Diameter smaller than the tube



→ Lateral oscillation

Wave length

$$\lambda_c = 2\pi L_c$$

$$L_c = \frac{\text{Capillary length}}{\sqrt{\Delta\rho g}}$$

$$L_c = \sqrt{\frac{\gamma}{\Delta\rho g}}$$

γ → Surface tension coefficient
Δρg → Difference of density (air-liquid)

Drag coefficient

$$C_d = 6 + \frac{32}{Re}$$

Drag force

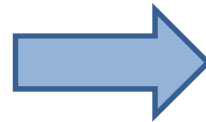
$$F_d = C_d \frac{\pi}{2} \rho U^2 R^2$$

$Re = \frac{UD}{\nu}$

Rise velocity of spherical cap

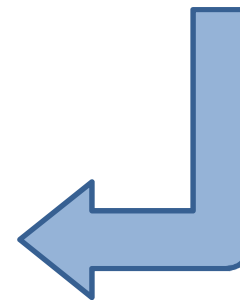
At the equilibrium: $F_d = B$

$$\left\{ \begin{array}{l} F_d = C_d \frac{\pi}{2} \rho U^2 R^2 \\ B = \rho g V \end{array} \right.$$



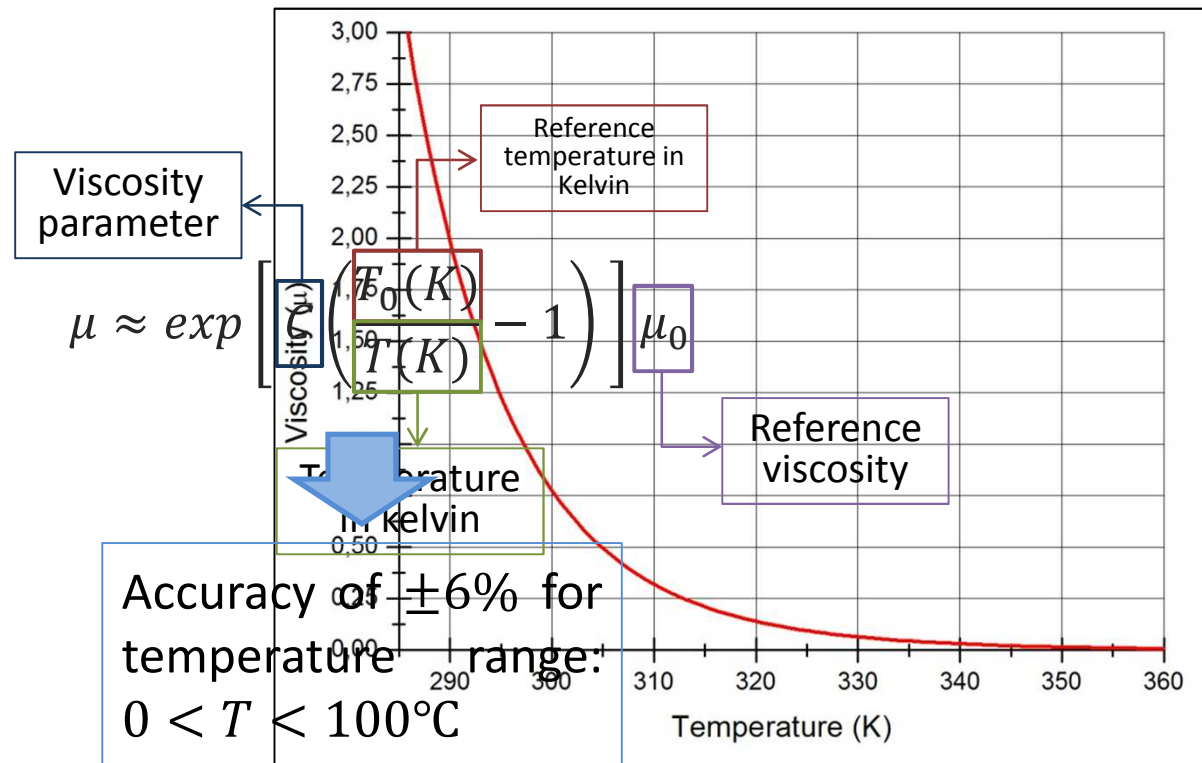
$$C_d \frac{\pi}{2} \rho U^2 R^2 = \rho g V$$

Finally: $U \left(\frac{32\nu}{D} + 6U \right) = 2gV$



Influence of temperature

- The temperature acts changing the viscosity of the fluid and the density of the air inside the bubble.



Experimental description

Experiment
1

- Vary the volume of the bubble

Experiment
2

- Vary the temperature

Experiment
3

- Vary the diameter of the tube

Experiment
4

- Influence of surfactant

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Materials

- Burette 50 ml
- Pipette 10 ml
- Glass tube 250 ml
- Syringe 10 ml
- Rubber tube
- Camera
- Computer software's



Experiment 1: Variation of the volume

Volume

Temperature

Diameter



Tube diameter: 15 mm

Syringe: 20 ml

Fluid: Glycerin

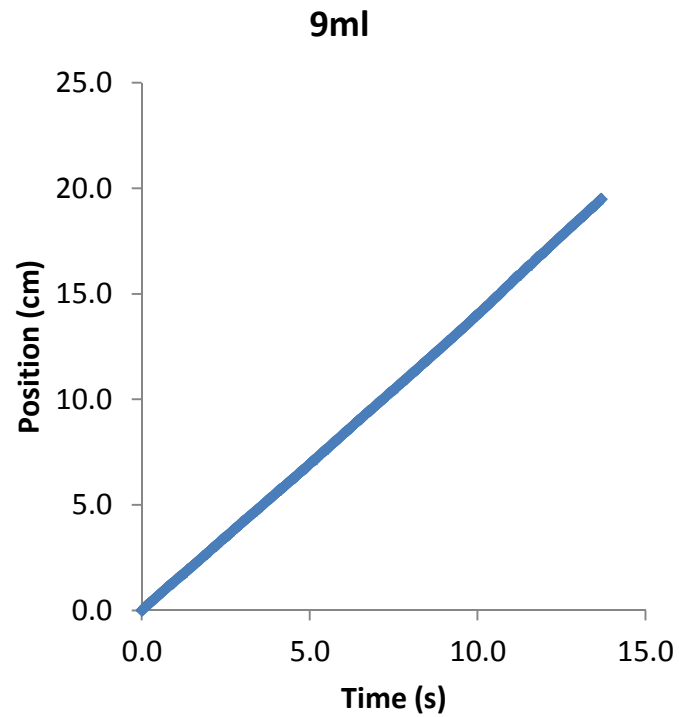
Temperature: 20°C

Source of errors:

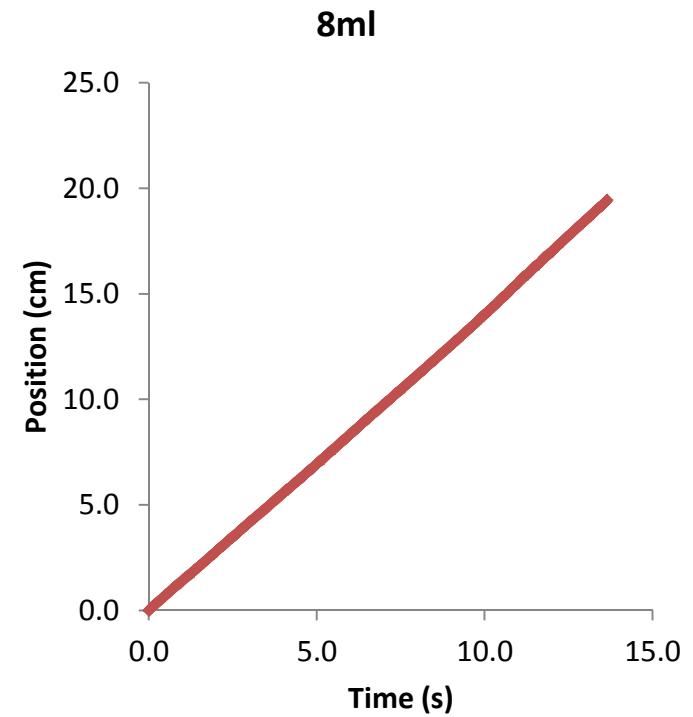
- Measuring ruler and conversion scale: $\pm 0.5\text{mm}$
- Volume of the syringe: $\pm 0.5\text{ ml}$

Experiment 1: Variation of the volume

- Volume
- Temperature
- Diameter



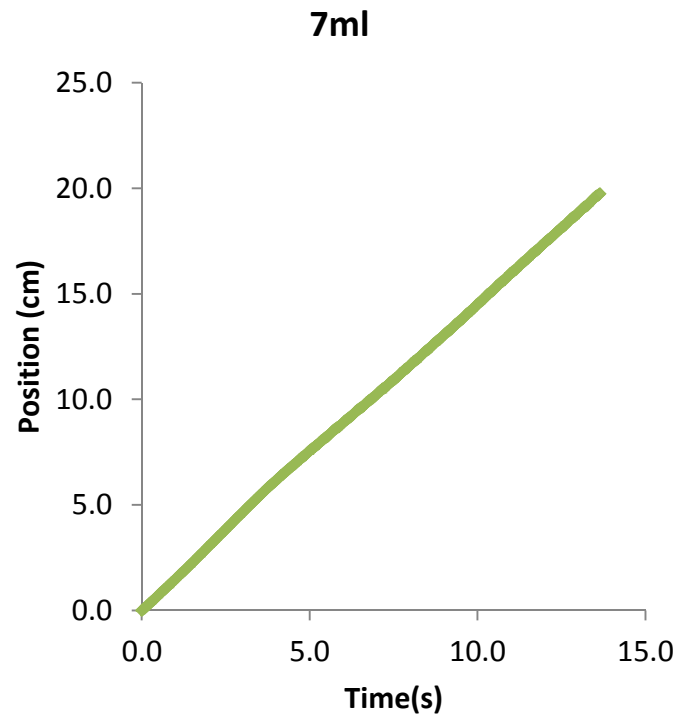
$$V_m = 0.01425 \text{ m/s}$$



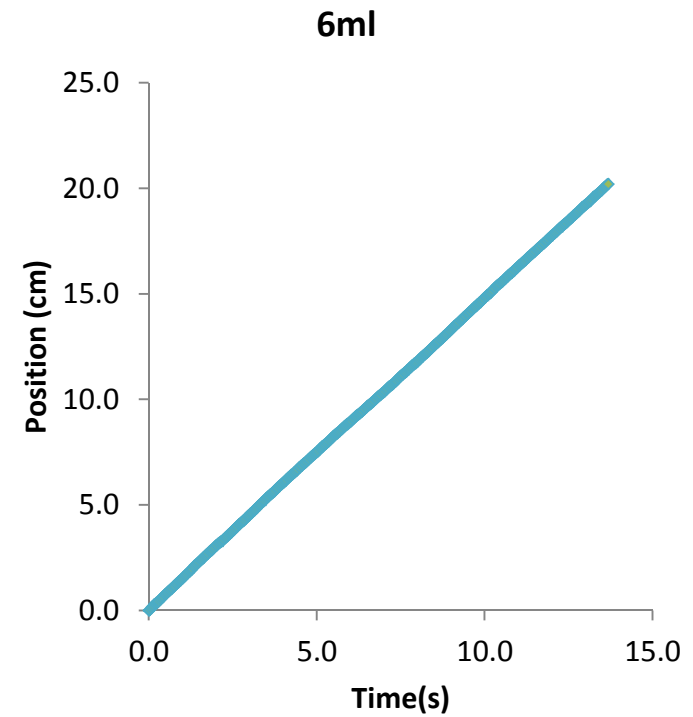
$$V_m = 0.01449 \text{ m/s}$$

Experiment 1: Variation of the volume

- Volume
- Temperature
- Diameter



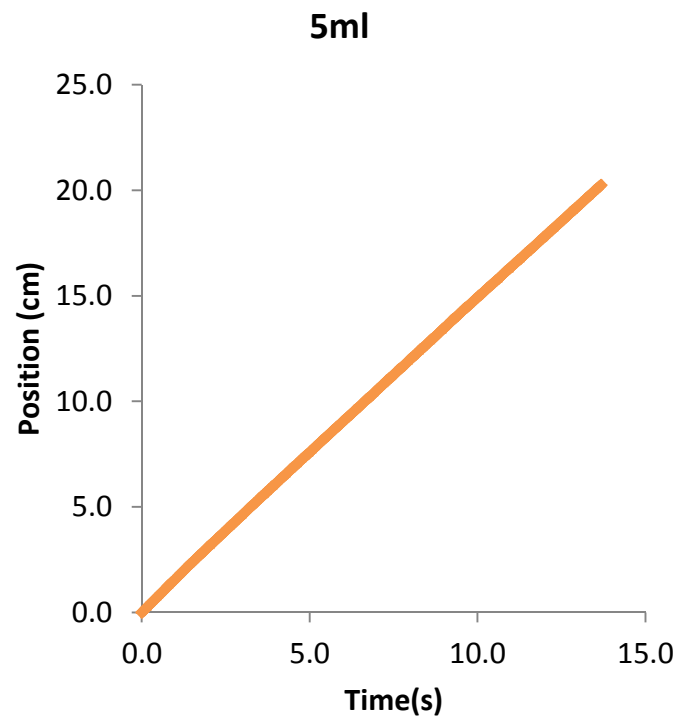
$$V_m = 0.01445 \text{ m/s}$$



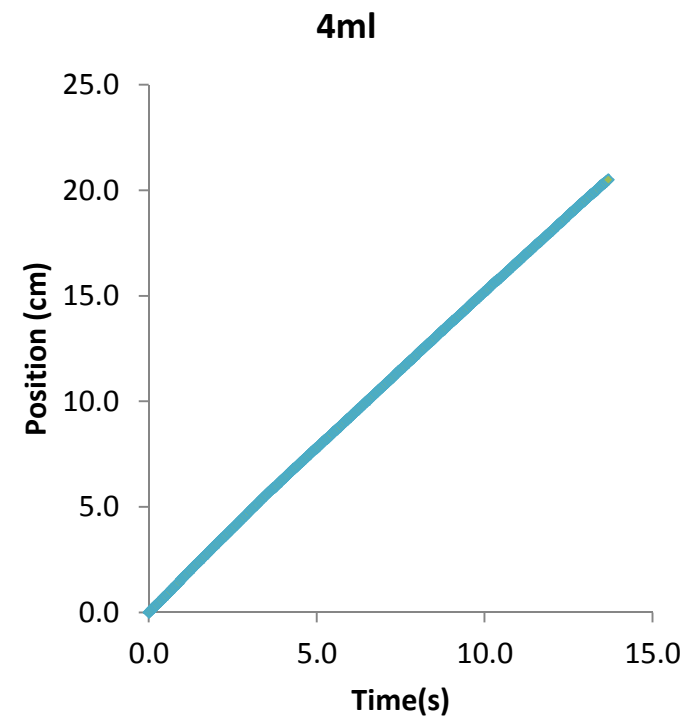
$$V_m = 0.01477 \text{ m/s}$$

Experiment 1: Variation of the volume

- Volume
- Temperature
- Diameter



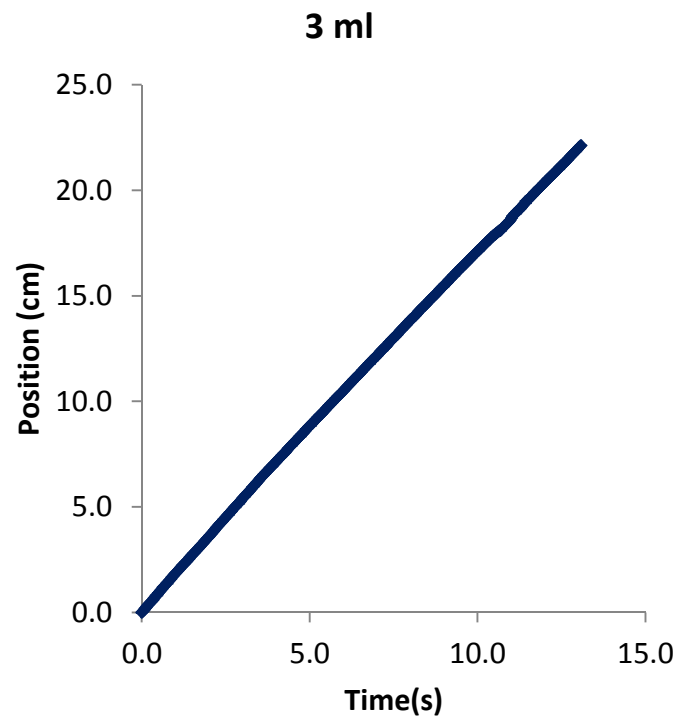
$$V_m = 0.01480 \text{ m/s}$$



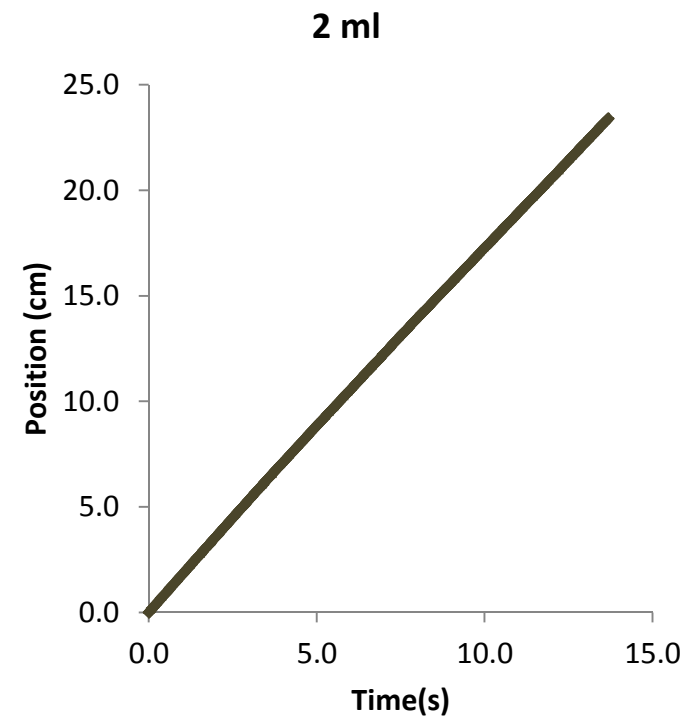
$$V_m = 0.01498 \text{ m/s}$$

Experiment 1: Variation of the volume

- Volume
- Temperature
- Diameter

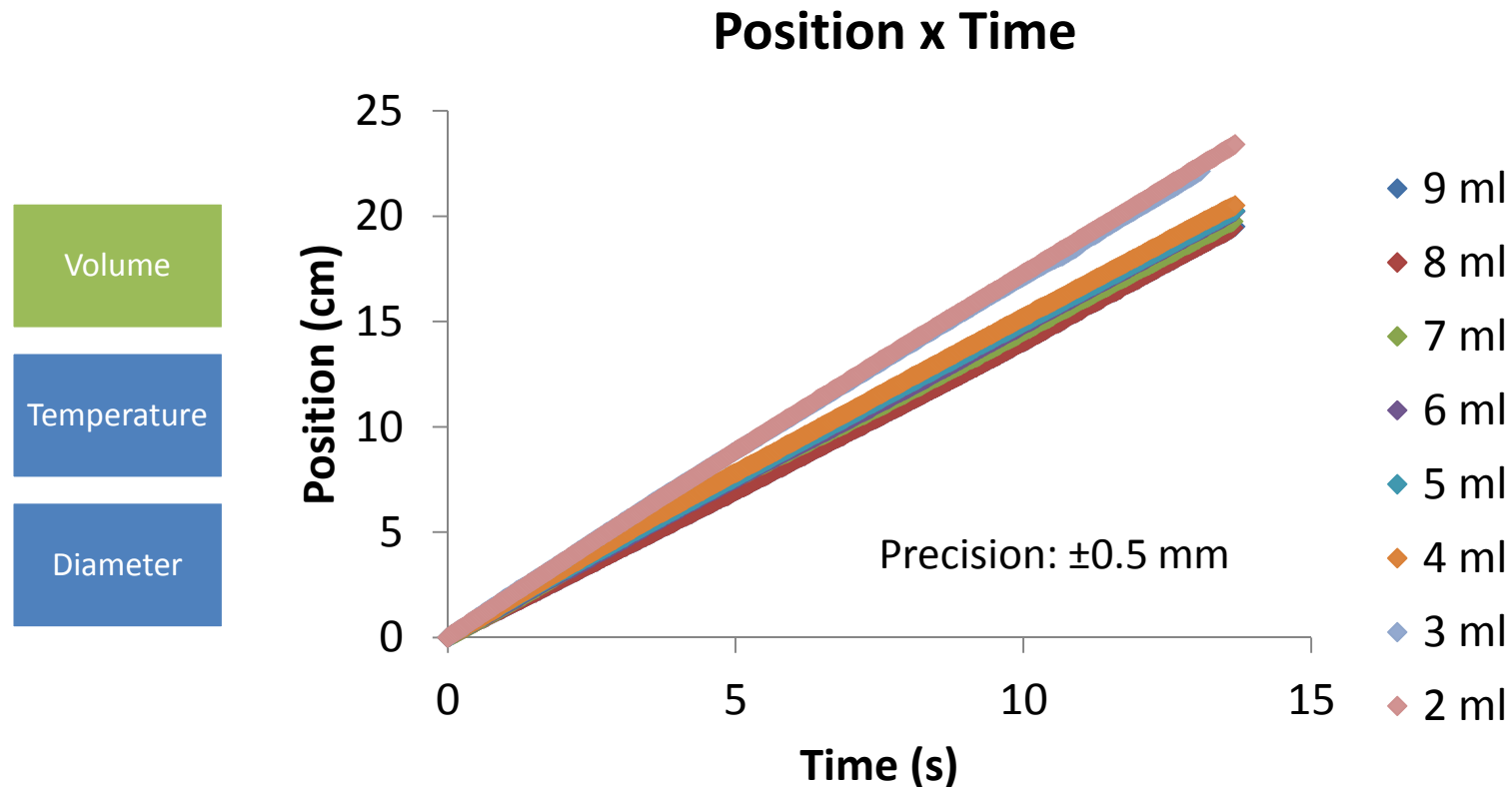


$$V_m = 0.01640 \text{ m/s}$$



$$V_m = 0.01710 \text{ m/s}$$

Experiment 1: Variation of the volume



Experiment 1: Variation of the volume

| Volume (ml) | Experimental velocity (m/s) | Theoretical velocity (m/s) |
|----------------|-----------------------------|----------------------------|
| 9 | 0.0142 | 0.0146 |
| 8 | 0.0144 | 0.0146 |
| 7 | 0.0144 | 0.0146 |
| 6 | 0.0147 | 0.0146 |
| 5 | 0.0148 | 0.0146 |
| 4 | 0.0149 | 0.0146 |
| 3 | 0.0164 | 0.0146 |
| 2 | 0.0171 | 0.0146 |
| Average | 0,0151 | 0.0146 |

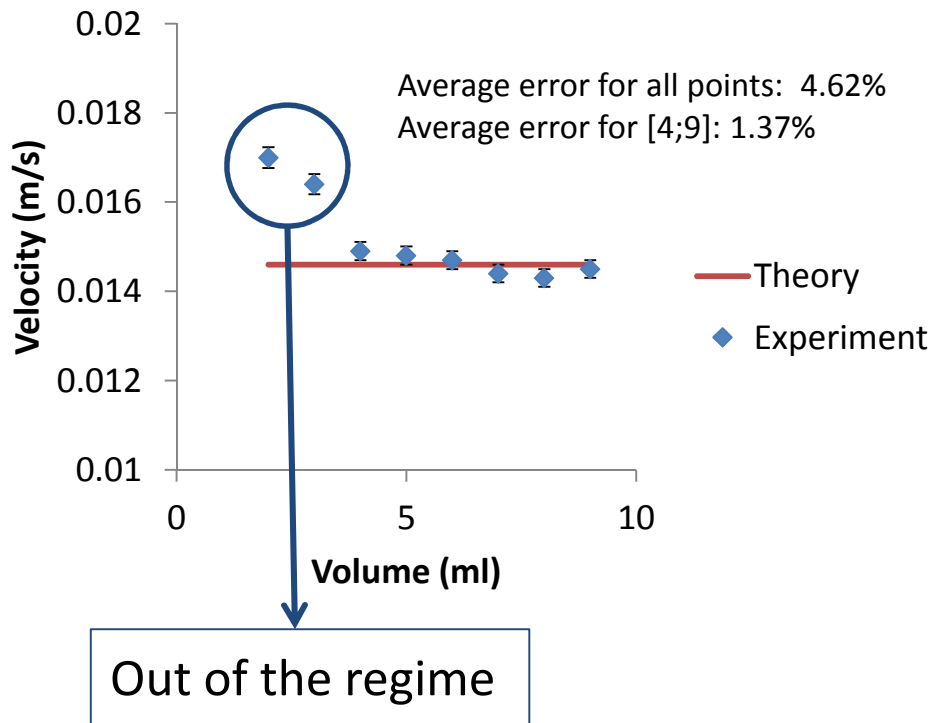
Volume

Temperature

Diameter

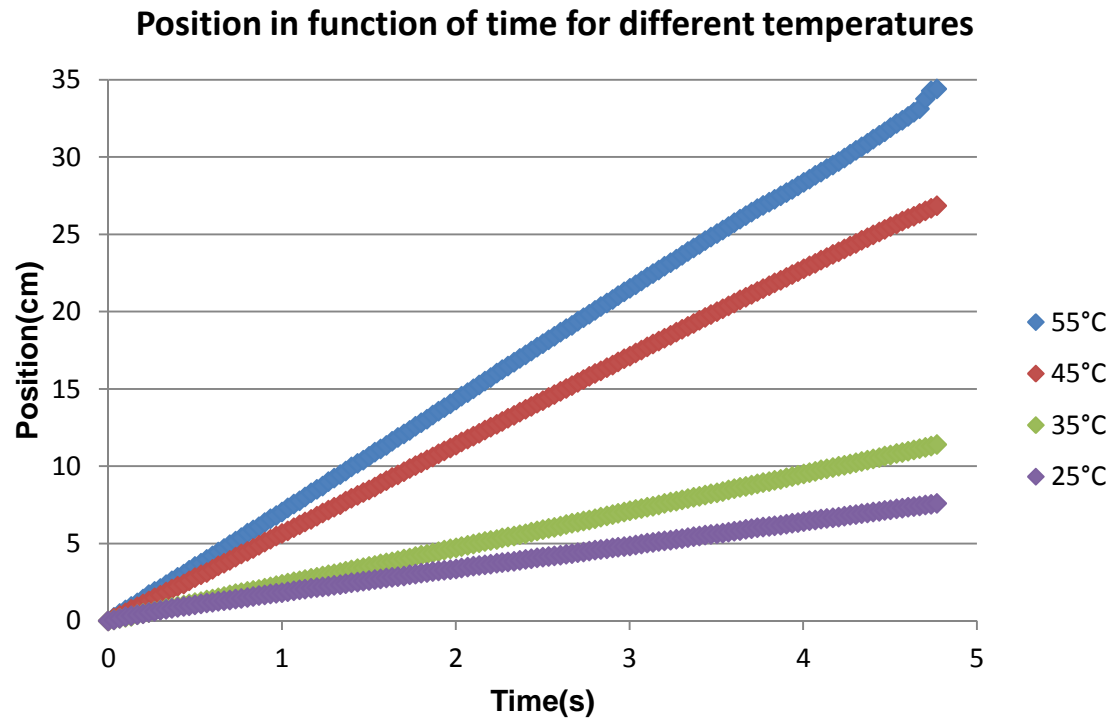


Experiment agrees with the theory



Experiment 2: Variation of the temperature

- Volume
- Temperature
- Diameter

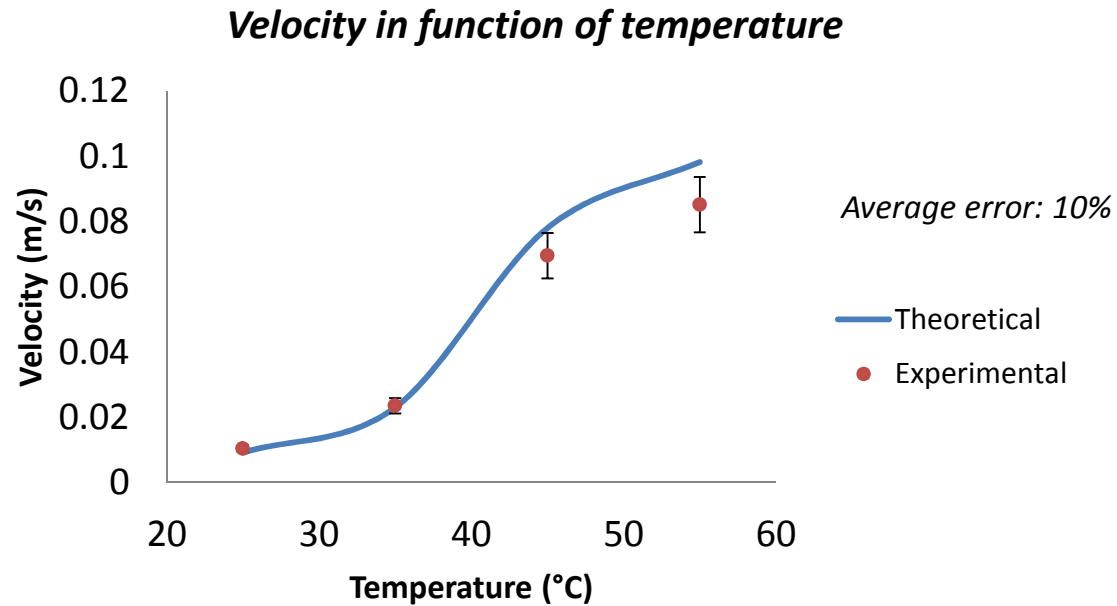


Experiment 2: Variation of the temperature

| | Temperature T ($^{\circ}\text{C}$) | Calculated Viscosity (m^2/s) $\times 10^{-4}$ | Predicted Velocity (m/s) | Experimental velocity |
|-------------|---|---|--|--------------------------|
| Volume | 55.0 | 0.409 | 0.0981 | 0.0850 |
| Temperature | 45.0 | 0.876 | 0.0779 | 0.0694 |
| Diameter | 35.0 | 1.973 | 0.0229 | 0.0234 |
| | 25.0 | 4.685 | 0.00910 | 0.0103 |

Experiment 2: Variation of temperature

- Volume
- Temperature
- Diameter

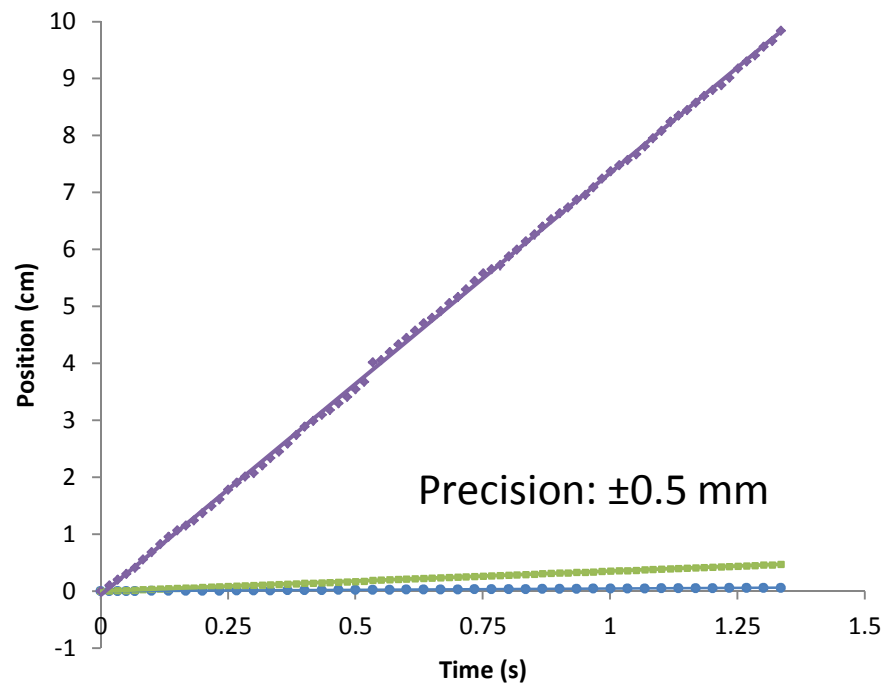


Experiment 3: Variation of the diameter

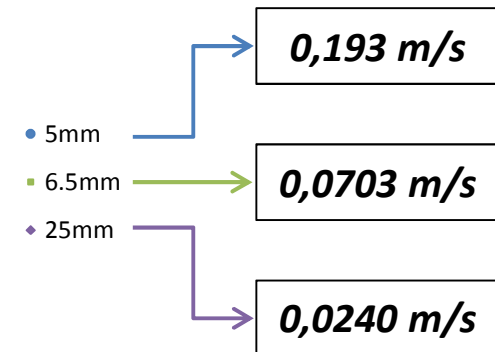
Fluid: Soy bean oil

Kinematic viscosity at 20°C (ν): 7.5×10^{-5}

- Volume
- Temperature
- Diameter



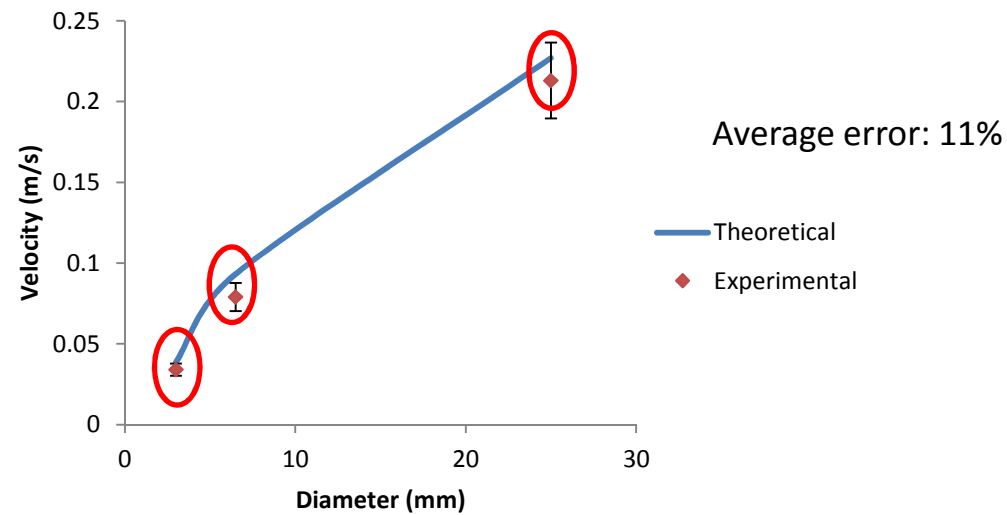
Experimental velocities



Experiment 3: Variation of the diameter

- Volume
- Temperature
- Diameter

| Diameter (mm) | Calculated Velocity (m/s) | Experimental Velocity (m/s) |
|---------------|---------------------------|-----------------------------|
| 25.0 | 0.2270 | 0.2130 |
| 6.5 | 0.0932 | 0.0790 |
| 5.0 | 0.0387 | 0.0340 |



Conclusion



Diameter of the tube



Viscosity



Temperature

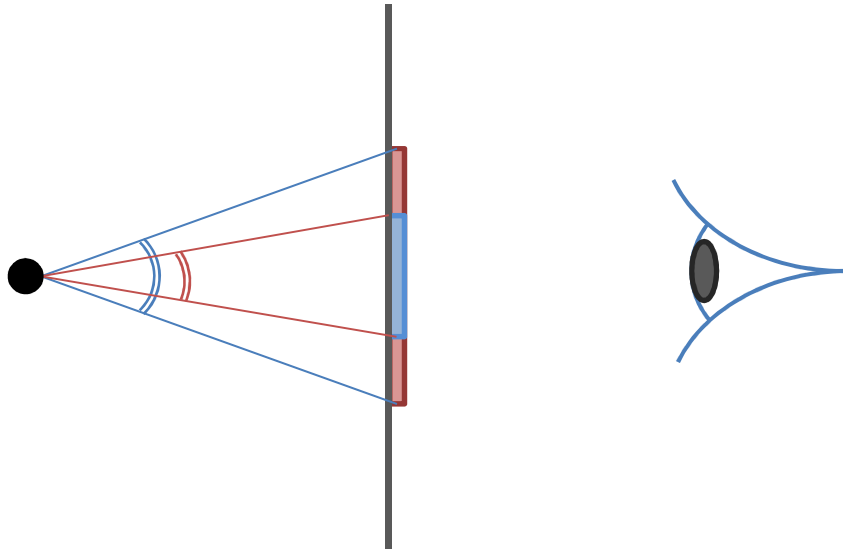


Diameter

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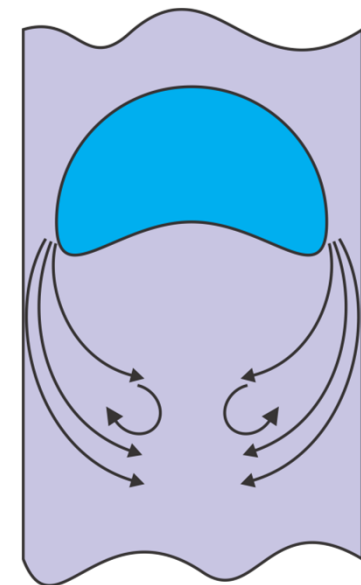
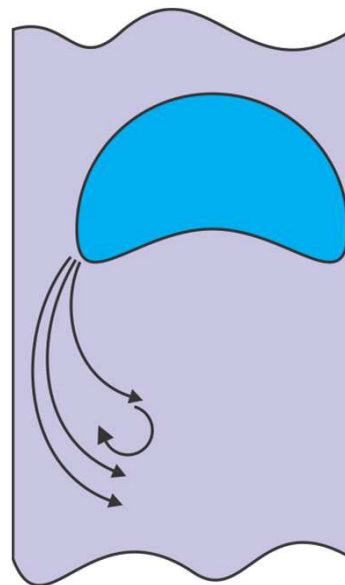
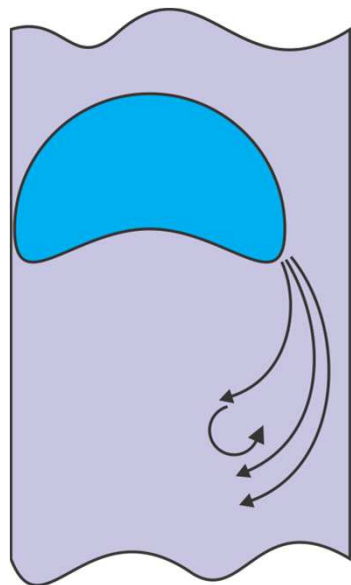
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Thank you!

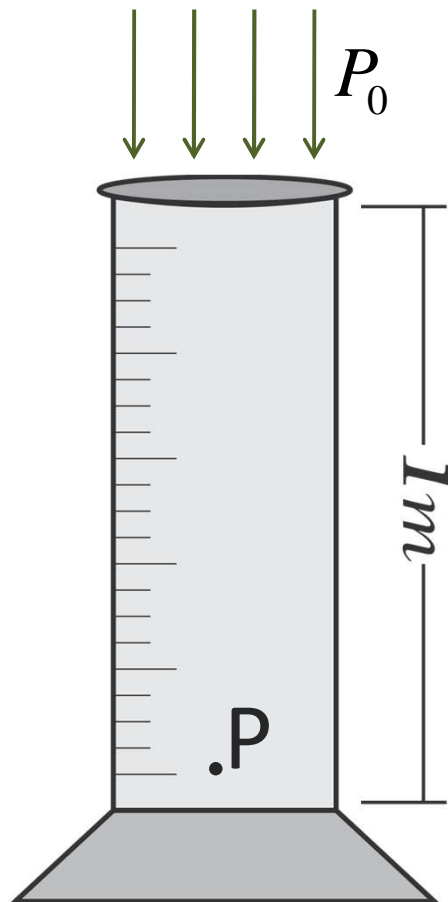


Lateral Flow

- For bubble measures comparable to the tube.



Pressure and volume variation



$$P_p = \rho \cdot g \cdot h + P_0$$

•For the following parameters:

- Fluid: Water
- Length of beaker: 1m

$$h = 0 \Rightarrow P = P_0$$

$$\Delta P = \rho \cdot g \cdot h = 1.10^3 Pa$$

$$\rho_{H_2O} = 10^3 \text{ kg/m}^3$$

$$P_0 = 1.10^5 \text{ Pa}$$

$$g = 9.81 \text{ m/s}^2$$

$$\frac{P_1 \cdot V_1}{T_1} = \frac{P_2 \cdot V_2}{T_2} \Rightarrow V_2 = 1.1 V_1$$

The weight of the bubble

•Considering a bubble with a volume of $2 \times 10^{-5} \text{m}^3$ (20mL):

Buoyancy
Weight

$$B = \rho_l V g$$

$$B = 10^3 \times 2 \times 10^{-5} \times 10 = 2 \times 10^{-1}$$

$$\left| \begin{array}{l} W = mg \\ \rho_g = m/V \end{array} \right. \Rightarrow W = \rho_g V g = 2.4 \times 10^{-4}$$

Relation
between them

$$\frac{W}{B} = \frac{2.4 \times 10^{-4}}{2 \times 10^{-1}} = 1.2 \times 10^{-3}$$

Conclusion

$$W = 0.6\% \text{ of } B, \text{ so } W \approx 0$$



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- <http://www.pmmh.espci.fr/~jbico/TP/taylor50bulle.pdf>

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| Fluid (l) | C | Fluid (l) | C |
|-----------|------|-----------|------|
| Ammonia | 1.05 | Freon 12 | 1.76 |
| Ethanol | 5.72 | Benzene | 4.34 |
| Gasoline | 3.68 | Mercury | 1.07 |
| Glycerin | 28.0 | Methanol | 4.63 |